

AMENDMENTS TO THE CLAIMS

1. – 7. (Cancelled)

8. (Currently Amended) A process for producing bisphenol A comprising condensing phenol and acetone in the presence of, as a catalyst, an acid type ion exchange resin which is modified in part with a sulfur-containing amine compound, wherein said condensing is performed in reaction equipment which comprises at least two reactors in series, and wherein an ion exchange resin having a modification rate in the range of 26 to 65 mol% is used for a methanol concentration in acetone being in the range of 700 to 8000 ppm by weight.

9. (Previously Presented) The process for producing bisphenol A according to Claim 8, wherein said acid type ion exchange resin is strongly acidic sulfonic acid type ion exchange resin.

10. (Previously Presented) The process for producing bisphenol A according to Claim 8, wherein the sulfur-containing amine compound is at least one species selected from the group consisting of mercaptoalkylpyridines, mercaptoalkylamines, thiazolidines and aminothiophenol.

11. (Previously Presented) The process for producing bisphenol A according to Claim 10, wherein the mercaptoalkylamine is 2-mercaptoethylamine and the thiazolidine is 2-2-dimethylthiazolidine.

12. (Currently Amended) A process for producing bisphenol A comprising condensing phenol and acetone in the presence of, as a catalyst, an acid type ion exchange resin which is modified in part with a sulfur-containing amine compound, wherein the phenol and acetone are subjected to condensation reaction in reaction equipment equipped with at least two reactors in series, and wherein said ion exchange resin has a different modification rate in accordance with the concentration of methanol in acetone, and wherein an ion exchange resin having a modification rate in the range of 10 to less than 20 mol% is used for a methanol concentration in acetone of lower than 250 ppm by weight, and an ion exchange resin having a modification rate in the range of 20 to 65 mol% is used for a methanol concentration in acetone being in the range of ~~250 to~~ 700 to 8000 ppm by weight.

13. (Previously Presented) The process for producing bisphenol A according to Claim 12, wherein the phenol and acetone are subjected to condensation reaction under the conditions including an acetone /phenol molar ratio in the range of 1/30 to 1/3 and a reaction temperature in the range of 40 to 150°C.

14. (Previously Presented) The process for producing bisphenol A according to Claim 12, wherein an ion exchange resin having a modification rate in the range of 26 to 65 mol% is used for a methanol concentration in acetone being in the range of 700 to 8000 ppm by weight.

15. (Previously Presented) The process for producing bisphenol A according to Claim 12, wherein said acid type ion exchange resin is strongly acidic sulfonic acid type ion

exchange resin.

16. (Previously Presented) The process for producing bisphenol A according to Claim 12, wherein the sulfur-containing amine compound is at least one species selected from the group consisting of mercaptoalkylpyridines, mercaptoalkylamines, thiazolidines and aminothiophenol.

17. (Previously Presented) The process for producing bisphenol A according to Claim 16, wherein the mercaptoalkylamine is 2-mercaptoethylamine and the thiazolidine is 2,2-dimethylthiazolidine.

SUPPORT FOR THE AMENDMENTS

Claims 1-7 were previously canceled.

Claims 8 and 12 have been amended.

The amendment of Claim 8 is supported by the specification as originally filed, for example at page 10, lines 19-24. The amendment of Claim 12 is supported by previously pending Claims 12 and 14, as well as the specification as originally filed, for example at page 8, lines 8-23.

No new matter has been added by the present amendment.